

*In the Claims*

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1. (Amended) A method of optimizing the efficiency of a combustion device ~~such as a furnace, boiler, oven, or stove~~, comprising at least three ~~one~~ control zones, each of said control zones comprising at least one burner assembly, said method comprising:

- 5                   a) individually supplying fuel to each of said burner assemblies in each of said control zones;
- b) individually measuring a combustion characteristic of the collective combusted gas from said burner assemblies in each of said control zones; and
- c) individually adjusting the flow of air to each of said burner
- 10 assemblies in each of said control zones in response to the value of said combustion characteristic corresponding to each of said control zones to keep the value of each of said combustion characteristics within a predetermined range.

2. A method in accordance with claim 1 wherein said combustion characteristic comprises a component selected from the group consisting of oxygen concentration, carbon monoxide concentration, carbon dioxide concentration, and combinations thereof.

3. A method in accordance with claim 1 wherein said combustion characteristic is oxygen concentration.

4. A method in accordance with claim 3 wherein the step of individually adjusting the flow of air to each of said burner assemblies in each of said control zones of step c) is performed such that the oxygen concentration in said collective combusted gas for each of said control zones is in the range of from about

5 0.5 to about 5.0 volume %, based on the total volume of said collective combusted gas.

5 5. A method in accordance with claim 3 wherein the step of individually adjusting the flow of air to each of said burner assemblies in each of said control zones of step c) is performed such that the oxygen concentration in said collective combusted gas for each of said control zones is in the range of from about 1.0 to about 3.0 volume %, based on the total volume of said collective combusted gas.

5 6. A method in accordance with claim 3 wherein the step of individually adjusting the flow of air to each of said burner assemblies in each of said control zones of step c) is performed such that the oxygen concentration in said collective combusted gas for each of said control zones is in the range of from 1.5 to 2.0 volume %, based on the total volume of said collective combusted gas.

7. A method in accordance with claim 1 wherein said combustion characteristic is carbon dioxide concentration.

5 8. A method in accordance with claim 7 wherein the step of individually adjusting the flow of air to each of said burner assemblies in each of said control zones of step c) is performed such that the carbon dioxide concentration in said collective combusted gas for each of said control zones is greater than about 2.0 volume %, based on the total volume of said collective combusted gas.

9. A method in accordance with claim 7 wherein the step of individually adjusting the flow of air to each of said burner assemblies in each of said control zones of step c) is performed such that the carbon dioxide concentration in

5 said collective combusted gas for each of said control zones is greater than about 5.0  
volume % , based on the total volume of said collective combusted gas.

10. A method in accordance with claim 7 wherein the step of  
individually adjusting the flow of air to each of said burner assemblies in each of said  
control zones of step c) is performed such that the carbon dioxide concentration in  
said collective combusted gas for each of said control zones is greater than about 10.0  
5 volume %, based on the total volume of said collective combusted gas.

11. A method in accordance with claim 1 wherein said combustion  
characteristic is carbon monoxide concentration.

12. A method in accordance with claim 11 wherein the step of  
individually adjusting the flow of air to each of said burner assemblies in each of said  
control zones of step c) is performed such that the carbon monoxide concentration in  
said collective combusted gas for each of said control zones is less than about 1000  
5 ppmv, based on the total volume of said collective combusted gas.

13. A method in accordance with claim 11 wherein the step of  
individually adjusting the flow of air to each of said burner assemblies in each of said  
control zones of step c) is performed such that the carbon monoxide concentration in  
said collective combusted gas for each of said control zones is less than about 500  
5 ppmv, based on the total volume of said collective combusted gas.

14. A method in accordance with claim 11 wherein the step of  
individually adjusting the flow of air to each of said burner assemblies in each of said  
control zones of step c) is performed such that the carbon monoxide concentration in

5 said collective combusted gas for each of said control zones is substantially 0 ppmv,  
based on the total volume of said collective combusted gas.

15. (Amended) A method of optimizing the efficiency of a  
combustion device ~~such as a furnace, boiler, oven, or stove,~~ comprising at least three  
~~one~~ control zones, each of said control zones comprising at least one burner assembly,  
said method comprising:

5 a) individually supplying fuel to each of said burner assemblies in each  
of said control zones;

10 b) individually supplying primary air to each of said burner assemblies  
in each of said control zones for mixture and at least partial combustion with said fuel  
supplied thereto thereby producing a separate intermediate combustion product for  
each of said burner assemblies;

c) individually supplying secondary air to each of said burner  
assemblies in each of said control zones for mixture with said intermediate  
combustion product for further combustion thereby producing a combusted gas stream  
for each of said burner assemblies;

15 d) individually measuring a combustion characteristic of the collective  
combusted gas from said burner assemblies in each of said control zones wherein said  
combustion characteristic is selected from the group consisting of oxygen  
concentration, carbon monoxide concentration, carbon dioxide concentration, and  
combinations thereof; and

20 e) individually adjusting the flow of said primary air and individually  
adjusting the flow of said secondary air to each of said burner assemblies in each of

said control zones in response to the value of said combustion characteristic corresponding to each of said control zones to keep the value of each of said combustion characteristics within a predetermined range.

16. A method in accordance with claim 15 wherein the flow of said primary air to each of said burner assemblies is adjusted in response to the value of said combustion characteristic corresponding to each of said control zones first, followed by adjustment of the flow of said secondary air, as needed, in order to keep the value of each of said combustion characteristics within said predetermined range.

17. ~~Canceled.~~

18. A method in accordance with claim 15 wherein said combustion characteristic is oxygen concentration.

19. A method in accordance with claim 18 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed such that the oxygen concentration of said collective combusted gas corresponding to each of said control zones is in the range of from about 0.5 to about 5.0 volume %, based on the total volume of said collective combusted gas.

20. A method in accordance with claim 18 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed such that the oxygen concentration of said collective combusted gas corresponding to each of said control zones is in the range of from about 1.0 to about 3.0 volume %, based on the total volume of said collective combusted gas.

21. A method in accordance with claim 18 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed such that the oxygen concentration of said collective combusted gas corresponding to each of said control zones is in the range of from 1.5 to 2.0 volume %, based on the total volume of said collective combusted gas.

22. A method in accordance with claim 15 wherein said combustion characteristic is carbon dioxide concentration.

23. A method in accordance with claim 22 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed such that the carbon dioxide concentration of said collective combusted gas corresponding to each of said control zones is greater than 2.0 volume %, based on the total volume of said collective combusted gas.

24. A method in accordance with claim 22 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed such that the carbon dioxide concentration of said collective combusted gas corresponding to each of said control zones is greater than about 5.0 volume %, based on the total volume of said collective combusted gas.

25. A method in accordance with claim 22 wherein the step of individually adjusting the flow of said primary air and of individually adjusting the flow of said secondary air to each of said burner assemblies of step e) is performed

such that the carbon dioxide concentration of said collective combusted gas  
5 corresponding to each of said control zones is greater than 10.0 volume % , based on  
the total volume of said collective combusted gas.

26. A method in accordance with claim 15 wherein said  
combustion characteristic is carbon monoxide concentration.

27. A method in accordance with claim 26 wherein the step of  
individually adjusting the flow of said primary air and of individually adjusting the  
flow of said secondary air to each of said burner assemblies of step e) is performed  
such that the carbon monoxide concentration of said collective combusted gas  
A/ 5 corresponding to each of said control zones is less than about 1000 ppmv, based on  
the total volume of said collective combusted gas.

28. A method in accordance with claim 26 wherein the step of  
individually adjusting the flow of said primary air and of individually adjusting the  
flow of said secondary air to each of said burner assemblies of step e) is performed  
such that the carbon monoxide concentration of said collective combusted gas  
5 corresponding to each of said control zones is less than about 500 ppmv, based on the  
total volume of said collective combusted gas.

29. A method in accordance with claim 26 wherein the step of  
individually adjusting the flow of said primary air and of individually adjusting the  
flow of said secondary air to each of said burner assemblies of step e) is performed  
such that said carbon monoxide concentration of said collective combusted gas  
5 corresponding to each of said control zones is substantially 0 ppmv, based on the  
total volume of said collective combusted gas.

30. (Amended) A combustion device comprising:

a) at least three ~~one~~-control zones, each of said control zones  
comprising at least one burner assembly;

5 b) at least one gas analyzer operably related to each of said control  
zones for receiving and analyzing samples of combusted gas from each of said control  
zones;

c) each of said burner assemblies comprising:

i) a fuel introduction means for introducing fuel into said burner  
assembly;

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*ent* 10 ii) a primary air introduction means for introducing primary air into  
said burner assembly for mixture and at least partial combustion with said fuel,  
thereby producing an intermediate combustion product; and

15 iii) a secondary air introduction means for introducing secondary air  
into said burner assembly for mixture and further combustion with said intermediate  
combustion product, thereby producing a combusted gas stream for each of said  
burner assemblies; and

20 d) control means operably related to said primary air introduction  
means, said secondary air introduction means, and said at least one gas analyzer, for  
adjusting the flow of primary air and the flow of secondary air to each of said burner  
assemblies in each of said control zones through said primary air introduction means  
and said secondary air introduction means, respectively, in response to the value of a  
combustion characteristic measured in the collective combusted gas streams  
corresponding to each of said control zones.



31. A combustion device as recited in claim 30 wherein said primary air introduction means comprises an adjustable primary air register and said secondary air introduction means comprises an adjustable secondary air register.

32. A combustion device as recited in claim 30 wherein said combustion characteristic is oxygen concentration.

33. A combustion device as recited in claim 30 wherein said combustion characteristic is carbon monoxide concentration.

34. A combustion device as recited in claim 30 wherein said combustion characteristic is carbon dioxide concentration.

35. A method of increasing the efficiency of a combustion device comprising the following steps:

- 5
- a) providing the combustion device of claim 30
  - b) introducing fuel into each of said burner assemblies in each of said control zones via said fuel introduction means;
  - c) introducing primary air into said burner assemblies in each of said control zones via said primary air introduction means for mixture and at least partial combustion with said fuel thereby producing an intermediate combustion product;
  - d) introducing secondary air into said burner assemblies in each of said control zones via said secondary air introduction means for mixture and further combustion with said intermediate combustion product thereby producing a combusted gas stream for each of said burner assemblies;
  - e) individually measuring the value of a combustion characteristic in the collective combusted gas streams corresponding to each of said control zones;
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15 f) adjusting the flow of said primary air and the flow of said secondary  
air to each of said burner assemblies in each of said control zones through said  
primary air introduction means and said secondary air introduction means,  
respectively, in response to the value of said combustion characteristics measured in  
step e) corresponding to each of said control zones.

36. A method in accordance with claim 35 wherein the flow of said  
primary air to each of said burner assemblies in each of said control zones is adjusted  
via said control means in response to the value of said combustion characteristic  
corresponding to each of said control zones first, followed by adjustment of the flow  
5 of said secondary air, as needed, via said control means in order to keep the value of  
each of said combustion characteristics within a predetermined range.

37. A method in accordance with claim 35 wherein the step of  
adjusting the flow of said primary air and the flow of said secondary air to each of  
said burner assemblies of step f) is performed such that the oxygen concentration in  
the collective combusted gas for each of said control zones is in the range of from  
5 about 0.5 to about 5.0 volume %, based on the total volume of said collective  
combusted gas.

38. A method in accordance with claim 35 wherein the step of  
adjusting the flow of said primary air and the flow of said secondary air to each of  
said burner assemblies of step f) is performed such that the oxygen concentration in  
the collective combusted gas for each of said control zones is in the range of from  
5 about 1.0 to about 3.0 volume %, based on the total volume of said collective  
combusted gas.

39. A method in accordance with claim 35 wherein the step of adjusting the flow of said primary air and the flow of said secondary air to each of said burner assemblies of step f) is performed such that the oxygen concentration in the collective combusted gas for each of said control zones is in the range of from 1.5 to 2.0 volume %, based on the total volume of said collective combusted gas.

40. A method in accordance with claim 35 wherein the step of adjusting the flow of said primary air and the flow of said secondary air to each of said burner assemblies of step f) is performed such that the carbon dioxide concentration in the collective combusted gas for each of said control zones is greater than about 2.0 volume % , based on the total volume of said collective combusted gas.

41. A method in accordance with claim 35 wherein the step of adjusting the flow of said primary air and the flow of said secondary air to each of said burner assemblies of step f) is performed such that the carbon dioxide concentration in the collective combusted gas for each of said control zones is greater than about 5.0 volume % , based on the total volume of said collective combusted gas.

42. A method in accordance with claim 35 wherein the step of adjusting the flow of said primary air and the flow of said secondary air to each of said burner assemblies of step f) is performed such that the carbon dioxide concentration in the collective combusted gas for each of said control zones is greater than 10.0 volume % , based on the total volume of said collective combusted gas.

43. A method in accordance with claim 35 wherein the step of adjusting the flow of said primary air and the flow of said secondary air to each of said burner assemblies of step f) is performed such that the carbon monoxide

concentration in the collective combusted gas for each of said control zones is less  
5 than about 1000 ppmv, based on the total volume of said collective combusted gas.

44. A method in accordance with claim 35 wherein the step of  
adjusting the flow of said primary air and the flow of said secondary air to each of  
said burner assemblies of step f) is performed such that the carbon monoxide  
concentration in the collective combusted gas for each of said control zones is less  
5 than about 500 ppmv, based on the total volume of said collective combusted gas.

45. A method in accordance with claim 35 wherein the step of  
adjusting the flow of said primary air and the flow of said secondary air to each of  
said burner assemblies of step f) is performed such that the carbon monoxide  
concentration in the collective combusted gas for each of said control zones is  
5 substantially 0 ppmv, based on the total volume of said collective combusted gas.

46. An apparatus suitable for analyzing combusted gas from a  
combustion device comprising a moveable cart physically supporting the following  
components:

a) a combusted gas probe;  
5 b) a free water knock-out vessel;  
c) a vacuum pump;  
d) a cooler containing a condenser and a condensed water knock-out  
vessel;

e) a combusted gas analyzer;  
10 wherein said free water knock-out vessel is connected in fluid flow  
communication with said combusted gas probe and with said vacuum pump, said

vacuum pump is connected in fluid flow communication with said condenser of said cooler; said condenser is connected in fluid flow communication with said condensed water knock-out vessel; and wherein said condensed water knock-out vessel is  
15 connected in fluid flow communication with said combusted gas analyzer.

47. A method in accordance with claim 1 wherein said measuring of each of said combustion characteristics of step b) is performed using the apparatus of claim 46; wherein said combusted gas probe is operably related to said combustion device for receiving combusted gas from said combustion device.

48. A method for analyzing combusted gas from a combustion device comprising:

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- a) supplying the apparatus of claim 46;
  - b) introducing a combusted gas stream from said combustion device to  
5 said free water knock-out vessel via said combusted gas probe;
  - c) permitting free water in said combusted gas stream to separate from the combusted gas stream for removal from said free water knock-out vessel;
  - d) passing said combusted gas stream to said vacuum pump;
  - e) passing said combusted gas stream to said condenser of said cooler  
10 for condensation of at least a portion of the combusted gas stream thereby forming a liquid phase and a gas phase which are passed to said condensed water knock-out vessel for separation; and
  - f) removing said liquid phase from said condensed water knock-out vessel and passing said gas phase to said combusted gas analyzer for analysis.

***Acknowledgment and Substance of Interview***

The interview courteously granted to Applicants' attorneys on April 22, 2003, is hereby acknowledged with appreciation.

The claims discussed during the interview were claims 1, 15, and 30. The prior art discussed were Lewis (U.S. 4,474,121), Yuino et al. (U.S. 5,630,714), and Sakai (57-90522).

During the interview, Applicants' attorney argued that Yuino turns the combustion on and off to various burners in order to control the temperature in a furnace, but the instant application adjusts the airflow to various burners in order to regulate a combustion characteristic. The Examiner stated that he will consider this argument.

The Applicants' attorney agreed to add language to claim 30 that one gas analyzer individually measures samples for each control zone to overcome the Sakai reference, and to argue that measuring samples from each control zone makes the combustion device operate in a more efficient manner.

Finally, Applicants' attorney agreed to add limitations regarding the type of combustion characteristics in order to overcome the Lewis reference.